

After recognizing the associative coefficient matrices, Danilevskii's method was used to evaluate each of these determinants. The results is

$$\frac{\partial |\lambda I - A|}{\lambda K} = (\lambda^4 + 6\lambda^3 + 11\lambda^2 + 6\lambda + 2) - (\lambda^4 + 6\lambda^3 + 11\lambda^2 + 6\lambda) \quad (13)$$

or

$$\frac{\partial |\lambda I - A|}{\partial K} = 2.0 \quad (14)$$

Thus,

$$\frac{\partial \lambda}{\partial K} = \frac{-2}{4\lambda^3 + 48\lambda^2 + 142\lambda + 116} \quad (15)$$

Evaluating Eq. (15) at the roots of the characteristic equation, the sensitivity coefficients can be obtained.

### Appendix

Danilevskii's method is a recursive technique for transforming any square matrix to the Frobenius form, i.e.,

$$P = \begin{bmatrix} 0 & 0 & \cdots & 0 & -d_0 \\ 1 & 0 & \cdots & 0 & -d_1 \\ 0 & 1 & \cdots & 0 & -d_2 \\ \vdots & \vdots & & & \\ 0 & 0 & & 1 & -d_{n-1} \end{bmatrix} \quad (A1)$$

Since the transformation is similar, the characteristic polynomials of Eq. (A1) and the original matrix are the same. It is easily verified that the characteristic polynomial of Eq. (A1) is

$$\Delta(\lambda) = |\lambda I - P| = \lambda^n + d_{n-1}\lambda^{n-1} + d_{n-2}\lambda^{n-2} + \dots + d_0 \quad (A2)$$

The recurrence process is as follows:

$$A_{k+1} = S_k^{-1} A_k S_k \quad k = 1, 2, \dots, n-1 \quad (A3)$$

The matrix to be transformed to the Frobenius form is  $A$ ; thus,  $A_1 = A$ . The matrix  $S_k$  is formed from the identity matrix by replacing the  $(k+1)$ th column by the  $k$ th column of  $A_k$ . The matrix,  $S_k^{-1}$  is formed from the identity matrix by replacing the  $(k+1)$ th column by the negative of the  $k$ th column of  $A_k$  divided by the  $(k+1)$ th element except for the  $(k+1)$ th element, which is the positive reciprocal.

The recurrence process above suggests matrix operations. However, these operations are so simple that the  $k$ th step of the process can be described as follows:

$$b_{ij} = \begin{cases} a_{ij}/a_{ik} & \text{for } i = k+1 \\ a_{ij} - a_{ik}b_{k+1,j} & \text{for } i \neq k+1 \end{cases} \quad (A4)$$

and

$$a'_{ij} = \begin{cases} \sum_{\ell=1}^n b_{i\ell} a_{\ell k} & \text{for } j = k+1 \\ b_{ij} & \text{for } j \neq k+1 \end{cases} \quad (A5)$$

where  $i = 1, 2, \dots, n$ , and  $j = 1, 2, \dots, n$ ;  $a_{ij}$  are the elements of the matrix  $A_k$ ;  $a'_{ij}$  are the elements of the matrix  $A_{k+1}$ ;  $b_{ij}$  are the elements of a "scratch-pad" matrix. The above are repeated  $n-1$  times. For more details on implementing Danilevskii's method, see Refs. 6 and 7.

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## Contaminants in a Gasdynamic Mixing Laser

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### Introduction

THE great potential of the gasdynamic mixing laser (GDML) as a high-energy system has been demonstrated by several groups, e.g., Refs. 1-4, to list but some of the more recent work. The basic idea that lies behind this conception is to produce separately thermally excited nitrogen and to inject cold carbon dioxide into a downstream region of lower temperature. By this means, advantage is taken of the facts that 1) the stagnation temperature can be raised to values far higher than the dissociation limit of  $\text{CO}_2$ , and 2) the freezing efficiency of a pure  $\text{N}_2$ -flow is extremely high. As a consequence, the available vibrational energy may be increased by approximately an order of magnitude as compared with typical values of premixed gasdynamic lasers (GDL).

In the work pertaining to the GDML, the nitrogen so far has been heated either in arc-heaters or in shock tubes. Both methods are useful and convenient in the course of basic investigations but may not be adequate in some applications. In those cases, a production of the hot  $\text{N}_2$  by chemical means would be preferable. On the other hand, each combustion process yields products in addition to  $\text{N}_2$ , which might have adverse effects upon the molecular kinetics involved in the GDML.

The effect of some contaminating additives like  $\text{O}_2$ ,  $\text{NO}$ ,  $\text{CO}$ ,  $\text{SO}_2$ , and  $\text{H}_2$  on small signal gain and laser power of a small-scale GDML has been investigated experimentally and is reported in this Note.

### Experiments and Discussions

The experimental apparatus used in this work is described in more detail in Ref. 4. Briefly, the  $\text{N}_2$  is heated in a d.c. arc-

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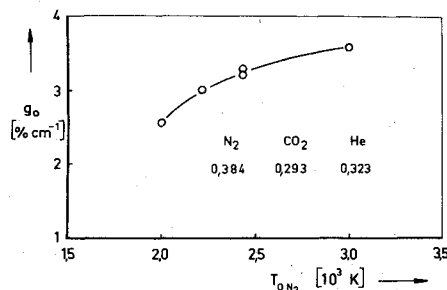


Fig. 1 Variation of small signal gain with stagnation temperature, pure  $\text{N}_2$  heated.

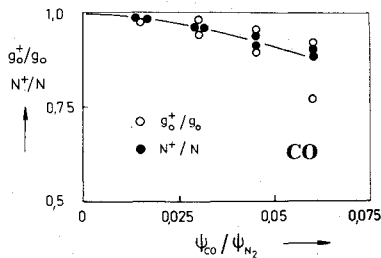


Fig. 2 Normalized small signal gain and laser power vs.  $\text{CO}$  mole fraction of  $\text{N}_2$ .

heater yielding typical stagnation conditions of  $T_0 \approx 2000$ – $3000 \text{ K}$  and  $p_0 \approx 4$ – $6 \text{ bar}$ . The expansion and mixing with the cold  $\text{CO}_2$  (pure or premixed with He or  $\text{H}_2$ ) takes place in a screen nozzle. The flow then enters the laser channel of  $3.5 \times 1.2 \text{ cm}^2$  cross section. At a distance  $8 \text{ cm}$  downstream of the nozzle exit measurements of small signal gain  $g_0$  (P20) and laser power  $N$  are performed. Figure 1 shows the dependence of  $g_0$  on  $T_0$  if pure  $\text{N}_2$  is used. It is noted that at approximately  $3000 \text{ K}$  values exceeding  $3.6 \text{ } \% \text{ cm}^{-1}$  are achieved and the curve indicates a further, even though small, rise with increasing temperature. The gas composition, as indicated in the graph, serves as a reference condition. Helium has been used as a deactivating agent throughout the experiments, although its presence is not fundamental for the function of this system. Comparative measurements show a 12% decrease of performance without He.

The various gas additives are heated by injecting them into a plenum chamber. It is of sufficient length to provide good mixing with the primary  $\text{N}_2$ -flow and to establish well-defined stagnation conditions. Data will be given for  $T_0 = 2800 \text{ K}$ .

The effect of  $\text{CO}_2$  and  $\text{H}_2\text{O}$  on the deactivation of  $\text{N}_2$  is well known and therefore not considered here. The addition of  $\text{O}_2$  and  $\text{NO}$  up to  $7.5\%$  to  $\text{N}_2$  does not reveal any deteriorating effect on gain and laser power. The effect of  $\text{CO}$  on the laser performance is shown in Fig. 2. Power and small signal gain are seen to decrease in approximately the same manner. The magnitude of the losses is in good agreement with the findings of Cassady et al.<sup>3</sup>

The results obtained with  $\text{SO}_2$  are presented in Fig. 3. Although there is some scatter in the  $g_0$ -data at higher mole fractions, the detrimental effect of  $\text{SO}_2$  on small signal gain and laser power becomes apparent. The decrease of laser power  $N^+$  (+ indicates conditions with addition of contaminant gases) is noticeably stronger than that of  $g_0^+$ . The dependence of  $g_0^+$  on the  $\text{SO}_2$  content is about the same as the one that was found in a shock-tube-driven premixed GDL at  $T_0 \approx 1500 \text{ K}$ .<sup>5</sup> A definite explanation of this behavior cannot be given at present. However, one has to note the close spacing between the vibrational levels of  $\text{N}_2$  at  $2331 \text{ cm}^{-1}$  and of  $\text{SO}_2$  ( $2\nu_1$ ) at  $2305 \text{ cm}^{-1}$ . It thus appears possible that the energy transfer from  $\text{N}_2$  to the upper laser level of  $\text{CO}_2$  at  $2349 \text{ cm}^{-1}$  becomes more inefficient as the number of molecules competing in resonant V–V transfer collisions is

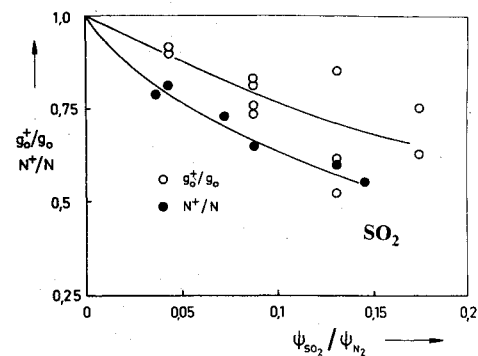


Fig. 3 Normalized small signal gain and laser power vs  $\text{SO}_2$  mole fraction of  $\text{N}_2$ .

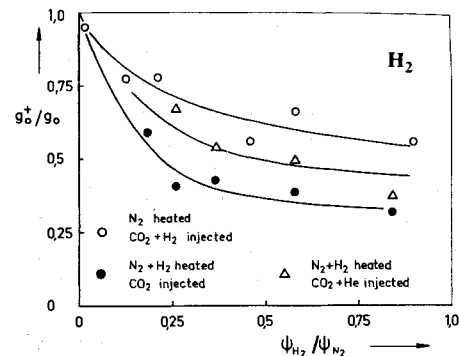


Fig. 4 Small signal gain vs  $\text{H}_2$  mole fraction of  $\text{N}_2$ .

increased. Furthermore, the lower laser level of  $\text{CO}_2$  at  $1388 \text{ cm}^{-1}$  is quite close to  $\text{SO}_2$  ( $\nu_3$ ) at  $1361 \text{ cm}^{-1}$  so that an interference with the depopulation process seems conceivable as well.

Finally, experiments have been performed concerning the effects caused by  $\text{H}_2$ . Some of the results obtained for a wide range of mole fractions are presented in Fig. 4. For the case of  $\text{H}_2$  being heated together with  $\text{N}_2$  and with pure  $\text{CO}_2$  injected into the expanding  $\text{N}_2/\text{H}_2$  flow, a rather dramatic decrease of small signal gain occurs already for  $\text{H}_2$  fractions below 20–25%. Using a mixture of  $\text{CO}_2$  and He instead of pure  $\text{CO}_2$ , the drop in  $g_0^+$  is less pronounced. In addition, a few measurements were made with pure  $\text{N}_2$ , but He substituted by  $\text{H}_2$  and injected together with  $\text{CO}_2$ . Here too, hydrogen causes a considerable loss of small signal gain, even at a very low  $\text{H}_2$  content of about 2%. Both experiments indicate a strong deactivating interference of  $\text{H}_2$  with the resonant  $\text{N}_2/\text{CO}_2$  energy level, whereas no evidence is found for a positive depopulation effect on the lower laser level. All together, these results confirm the generally recognized fact that  $\text{H}_2$  has no beneficial effect upon the laser performance.

### Conclusion

In conclusion, it is expected that a combustion-driven GDML will preserve its basic advantage of high specific energy as long as the amount of some contaminants (especially  $\text{SO}_2$ ,  $\text{H}_2$ ,  $\text{H}_2\text{O}$ ) does not exceed a few percent of the  $\text{N}_2$  flow.

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## Boundary-Layer Blockage with Mass Transfer

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### Nomenclature

- $b$  = mass-transfer parameter,  $2(\rho v)_w / \rho_e U_e C_{f0}$   
 $C_f$  = skin-friction coefficient  
 $F$  = streamwise variation of channel geometry, Eq. (12)  
 $f_1$  =  $-2V \times [1 - 2/b_{cr0}]$ , Eq. (18)  
 $f_2$  =  $-2V \times [1 + H_1 (1 - 2/b_{cr0}) + (1 - M_e^2) (d \ln U_e / d \ln x)]$ , Eq. (18)  
 $f_3$  =  $m S_{cr} d \ln U_e / dx - \psi d \ln C_{f0} / d \theta - 2V / C_{f0}$ , Eq. (22)  
 $h$  = height from wall to channel centerline  
 $H$  = shape factor,  $\delta^* / \theta$   
 $M$  = Mach number  
 $m$  = constant in Eq. (8), typically 1.75  
 $\dot{m}$  = mass flow rate  
 $Re$  = Reynolds number  
 $S$  = pressure gradient parameter,  $\theta d \ln U_e / dx$   
 $\bar{S}$  =  $S / S_{cr}$   
 $U$  = streamwise velocity  
 $v$  = transverse velocity  
 $V$  =  $(\rho v)_w / 2 \rho_e U_e \theta$   
 $W$  = spanwise channel dimension  
 $x$  = streamwise coordinate  
 $\delta^*$  = displacement thickness  
 $\kappa$  = constant in Eq. (2), typically 0.4  
 $\epsilon$  = pressure gradient parameter, Eqs. (6, 7, and 9)  
 $\rho$  = fluid density  
 $\theta$  = momentum thickness  
 $\psi$  = generalized skin friction modulator function  
 $\psi_b$  =  $(1 - b/b_{cr})^2$ , constant pressure, isothermal mass transfer  $\psi$   
 $\psi_p$  = zero mass transfer, isothermal pressure gradient  $\psi$ , Eq. (8)

### Subscripts

- $e$  = freestream conditions  
 $0$  = constant pressure, zero mass transfer  
 $1$  = variable pressure, zero mass transfer  
 $cr$  = critical value  
 $w$  = wall conditions

**C**ONSIDERATION of boundary-layer blockage effects generally involves data correlations or analytical formulations that utilize the local displacement thickness. Internal flows, for example at the entrance to diffusers, and external flows, on slender bodies whose flowfields are dominated by viscous-induced streamline deflection, follow this treatment. In both of these situations, boundary-layer

control (suction or blowing) has application in obtaining efficient designs and/or maintaining structural integrity.

The  $\delta^*$  distribution may be obtained through simple integral calculations utilizing the momentum equation

$$\frac{d\theta}{dx} + \frac{\theta}{U_e} \frac{dU_e}{dx} [H + 2 - M_e^2] = \frac{C_f}{2} + \frac{(\rho v)_w}{\rho_e U_e} \quad (1)$$

to obtain  $\theta$  and subsequently  $\delta^* = H\theta$ .

The results of Ref. 1 provide a method for modeling the effects of pressure gradient and wall temperature on  $C_f$  and  $H$  in a high-Reynolds-number turbulent flow. The effect of mass transfer on  $C_f$  in a constant-pressure isothermal flow also is presented. In addition, an approximate analysis of the influence of mass transfer on  $C_f$  in a constant-pressure nonisothermal flow is developed. However, the dependences of  $H$  and  $C_f$  on mass transfer in a pressure gradient are not addressed.

The purpose of this Note is to point out that, because of the origin of  $H$  as a definition based on  $\delta^*$  and  $\theta$ , the dependence of  $H$  on mass transfer may be exposed directly from considerations of mass continuity. In so doing, it is necessary to utilize only the physical interpretation of  $\delta^*$  and the fact that mass transfer appears as an explicit term in the momentum equation. A prerequisite to this approach is the development of an appropriate  $C_f$  model with mass transfer in a pressure gradient.

Large mass transfer rates are excluded from consideration in order to obtain a closed-form "linearized" solution. This is of particular relevance in diffuser blockage determination, wherein a small amount of system power is diverted to apply suction along a short segment of upstream boundary layer such that the increased diffuser recovery results in a net increase in system efficiency.

The zero-mass-transfer, constant-pressure shape factor is obtained<sup>1</sup> from the relationship

$$H_0 = 1 + \sqrt{2C_{f0}} / (\kappa - \sqrt{2C_{f0}}) \quad (2)$$

which extends to variable pressure flows through use of the following endpoint fitting formula:

$$(H_1 - 1) / (H_0 - 1) = [(H_{cr} - 1) / (H_0 - 1)]^{\bar{S}} \quad (3)$$

Both  $H_0$  and  $H_{cr}$  are affected by the degree of nonisothermality, as indicated by the results of Ref. 1.

A variety of skin-friction models for constant-pressure flows are available. The formula employed in Ref. 1,

$$C_{f0} = 2.0 / (2.5 \ln Re_0 + 3.8)^2 \quad (4)$$

provides generally useful results for smooth surfaces. Roughness amplification of this value may be obtained from the development in Ref. 2. Inclusion of pressure gradient effects is possible utilizing results from previously computed flows (see Fig. 28 of Ref. 1).

For constant-pressure flows, the combined effects of mass transfer and nonisothermality on  $C_f$  are approximated<sup>1</sup> by a superposition of their separate influences. The assumption is made here that the same can be done in variable-pressure flows, and, therefore, isothermal flow is considered for notational clarity.

In constant-pressure flows, the effect of mass transfer on  $C_f$  may be written as

$$C_f = C_{f0} \times \psi_b \quad (5)$$

where  $\psi_b$  is obtained from the integration of Eq. (4.2) of Ref. 1. In addition,  $b_{cr} = 4.0$ , as indicated from the integration when  $\psi = 0$ .

In the presence of pressure gradients, Eq. (5) is inappropriate, and inclusion of a *weak* pressure gradient

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